

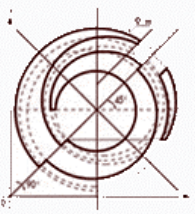
September 12, 2002

Combustion Technology Development Needs and Opportunities

Combustion Technology University Alliance Workshop, Salt
Fork Lodge, Cambridge, OH




John L. Marion

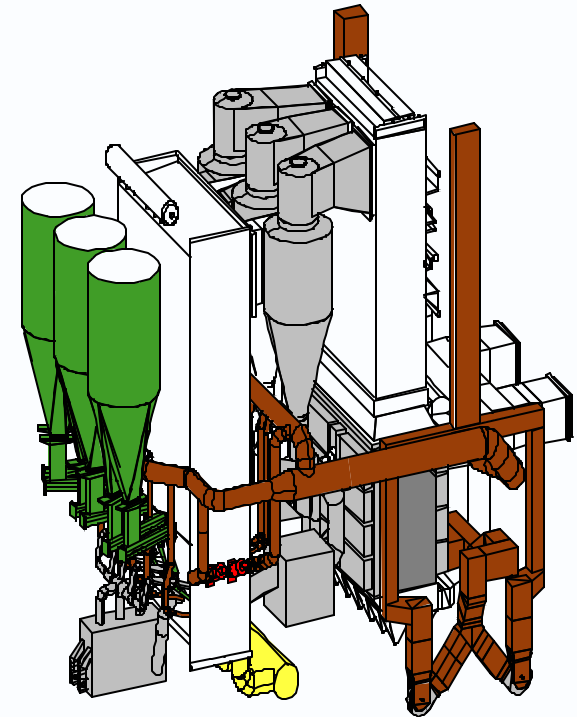
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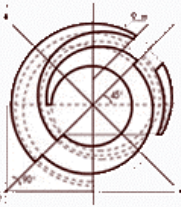
Roadmap for Combustion-based Power

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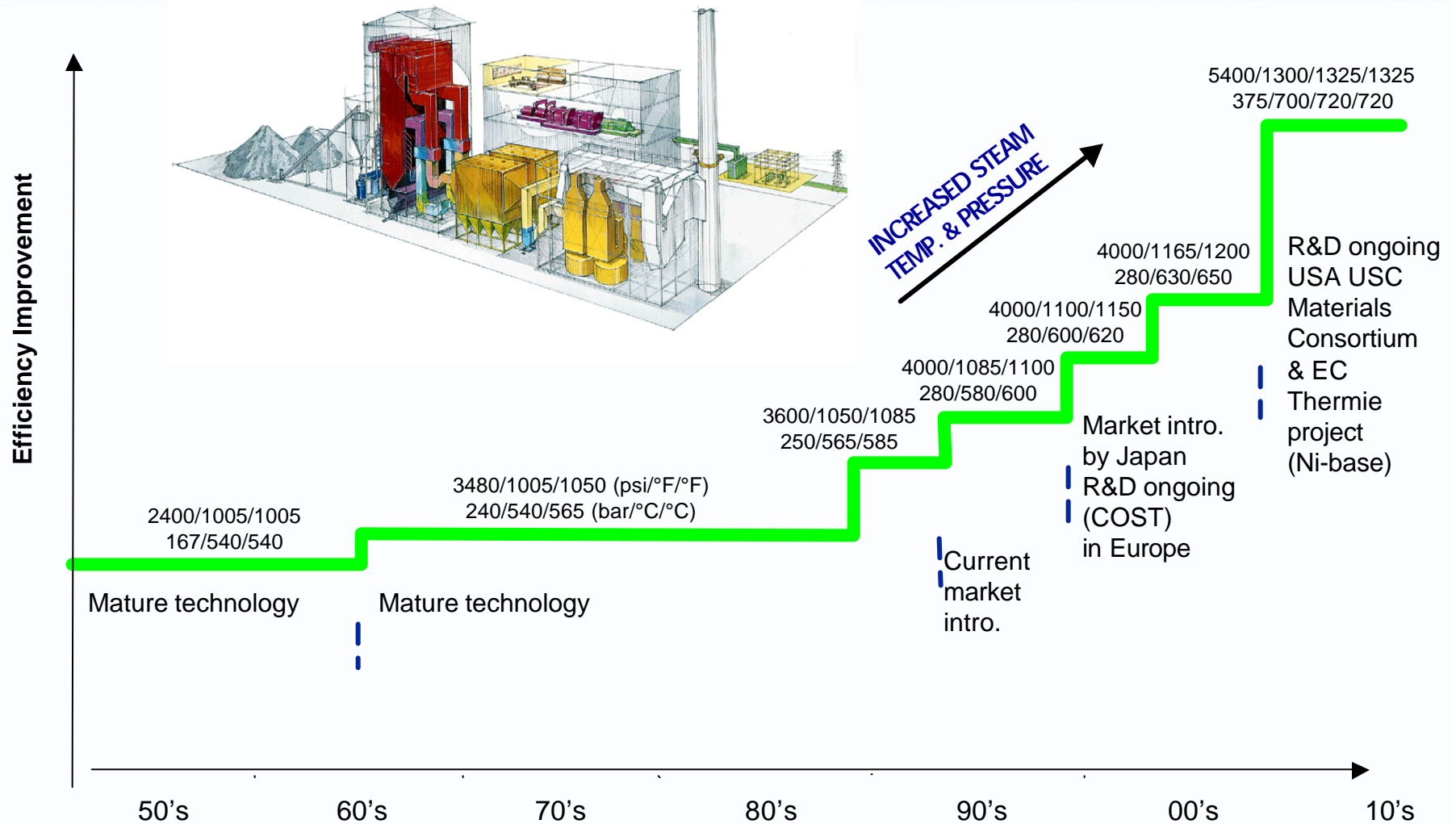
-  **Ultra-supercritical steam conditions**
 - increase efficiency
-  **Circulating Fluid Bed (CFB) and “advanced CFBs”**
 - low costs, low emissions, fuel flexibility
-  **CO2 Capture**
-  **Emissions controls**
 - for new and existing, and integrated and post



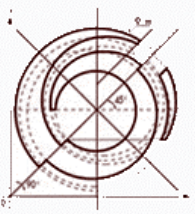
ALSTOM's view includes four (4) legs to advance coal combustion-based power technology



Ultra-supercritical technology Trend **ALSTOM**



Cost Effective Materials are Key



Partnership: Ultrasupercritical Materials

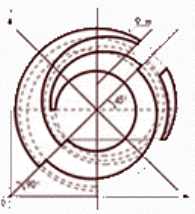
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- ✍ DOE, the State of Ohio Office of Coal Development and industry have teamed to develop next generation technology which will provide efficiency and environmental gains
- ✍ A uniquely qualified industry team - Energy Industry of Ohio, **all** the major US boiler manufacturers, a renowned national lab, Ohio organizations, and EPRI
- ✍ An aggressive goal - 1400°F steam temperature
 - Looks beyond Japanese and European practice and materials to where US alloys may be best



BABCOCK BORSIG POWER

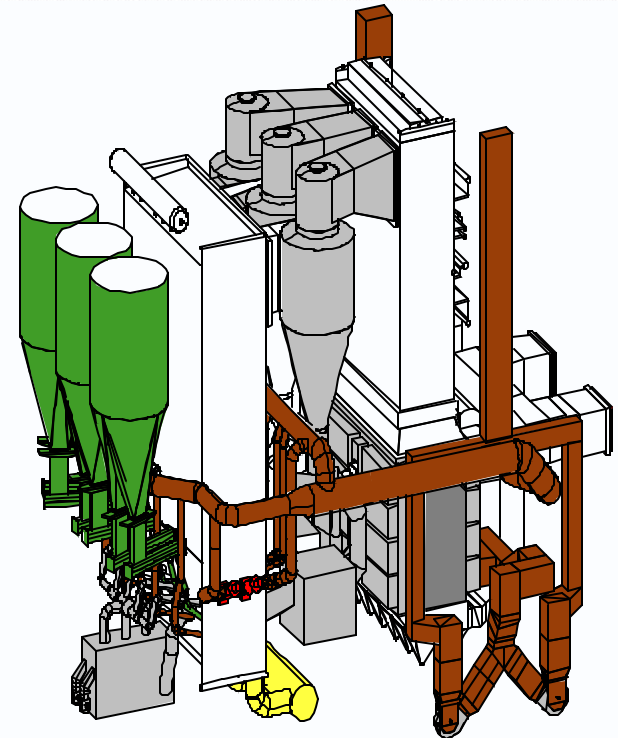
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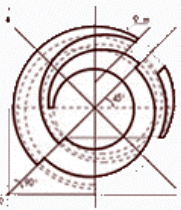
Circulating Fluidized Bed Power Plants Today

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- ✍ Utilize lower cost solid fuels which are difficult to burn
- ✍ Fuel flexibility enables low cost spot market purchases
- ✍ Inherent Low NO_x
 - Low combustion temperatures and staged combustion; also amenable to in-furnace (cyclone) ammonia injection for SNCR
 - NO_x emissions from 0.06 to 0.25 lbs/MM BTU
- ✍ Inherent Low SO_x as a result of limestone injection
 - Typical removals of 90 - 97%+; up to 98.5% with secondary equipment



Economic Utilization of Low Cost Fuels

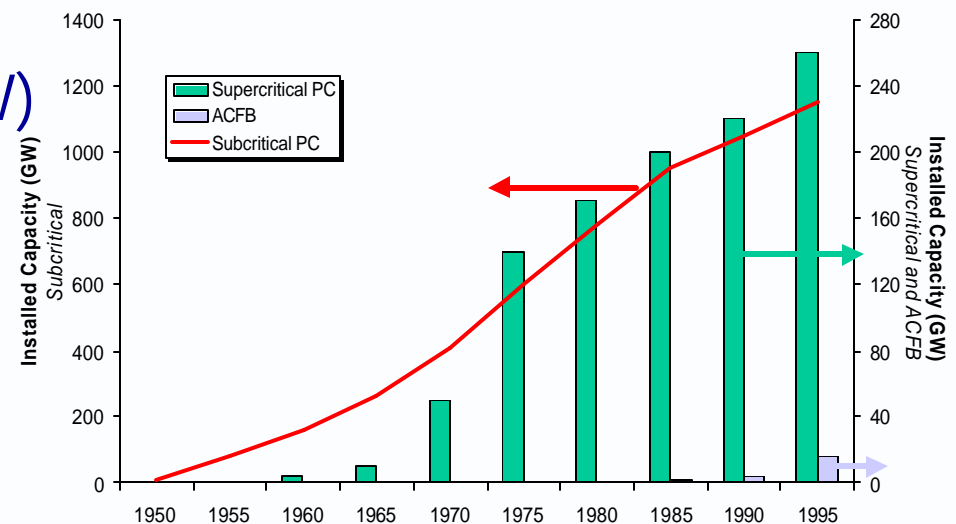


Future Circulating Fluidized Bed (CFB)

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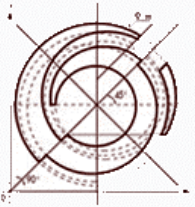
- ✍ Reduce Costs (new designs)
- ✍ Ultra Clean (integrated APC)
- ✍ Grow in Size (up to 600 MW)
- ✍ Improve Efficiency by Supercritical and USC conditions
- ✍ Enable Re-Powering
- ✍ Enable CO2 capture

Summary of Global Installed Coal Capacity for Sub-critical PC, Super-critical PC, and CFB boilers



JLM03/Combustion-DOE-Sept11'02.ppt

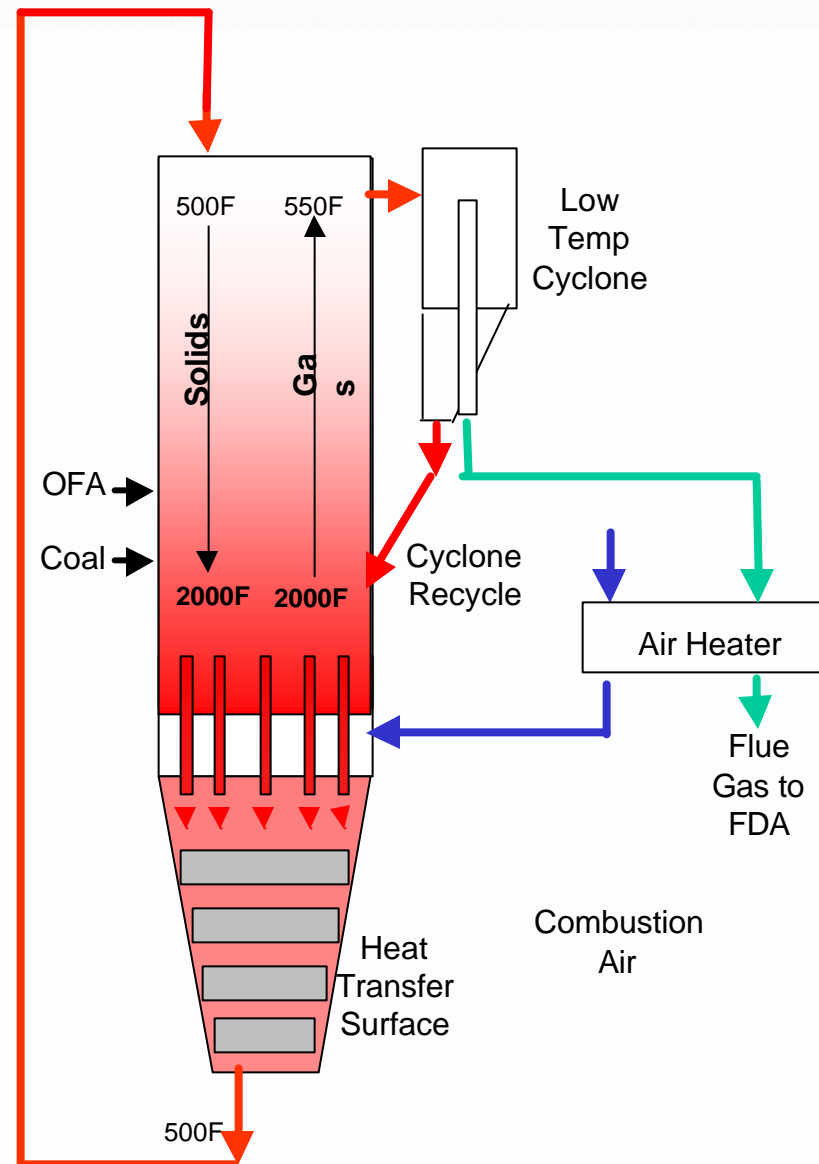
CFB's are early in the adoption and innovation curve

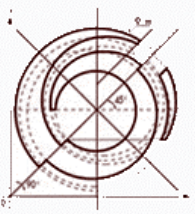


“Advanced CFB” or “Circulating Moving Bed [CMB]”

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- Separate heat transfer from combustion
- More effective surface allows supercritical steam conditions at lower cost
- Lower cost than ordinary CFB for conventional duty
- Lower auxiliary power
- Potential Pathway to in situ CO₂ capture





CO₂ Capture in Combustion Systems

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► “Tail-end” CO₂ capture

- adsorption/stripping process (MEA, MEA/MDEA, and physical absorbents)



► Oxygen combustion

- internal (membrane) or external (ASU) O₂

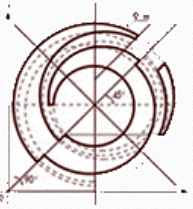
► Other options

- oxidation/reduction cycles
- carbonate capture
- chemical looping



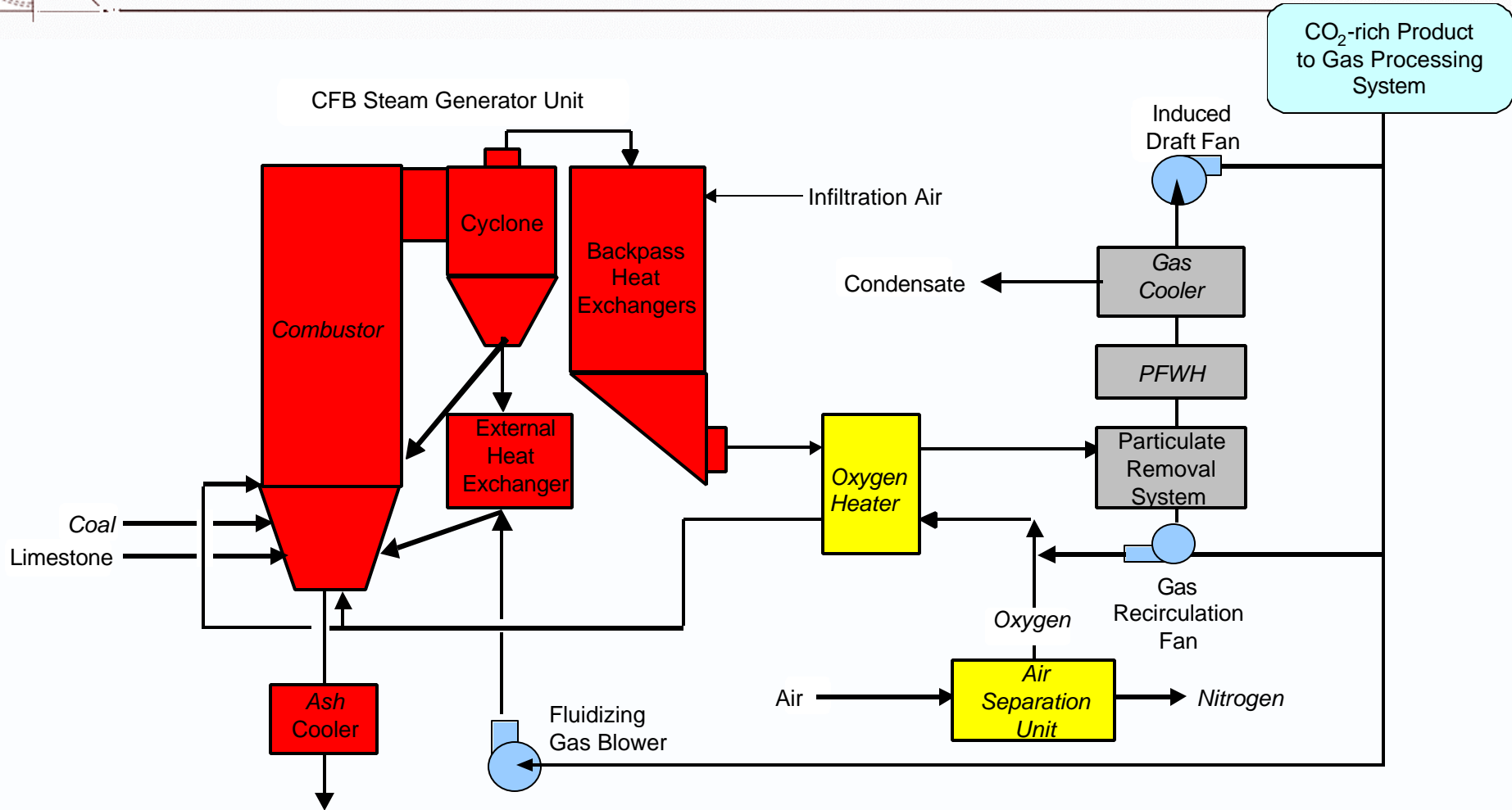
Innovative technology options just now emerging

For both combustion-based and gasification-based power

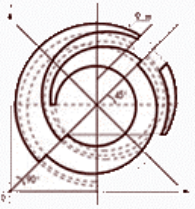


O₂ Fired CFB for CO₂ Capture

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Oxy-fuel combustion in a CFB requires less flue gas recycle in order to maintain combustion temperature



Carbonate Cycle for CO₂ Capture **ALSTOM**

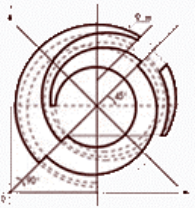
Below 750°C....



Above 1050°C....

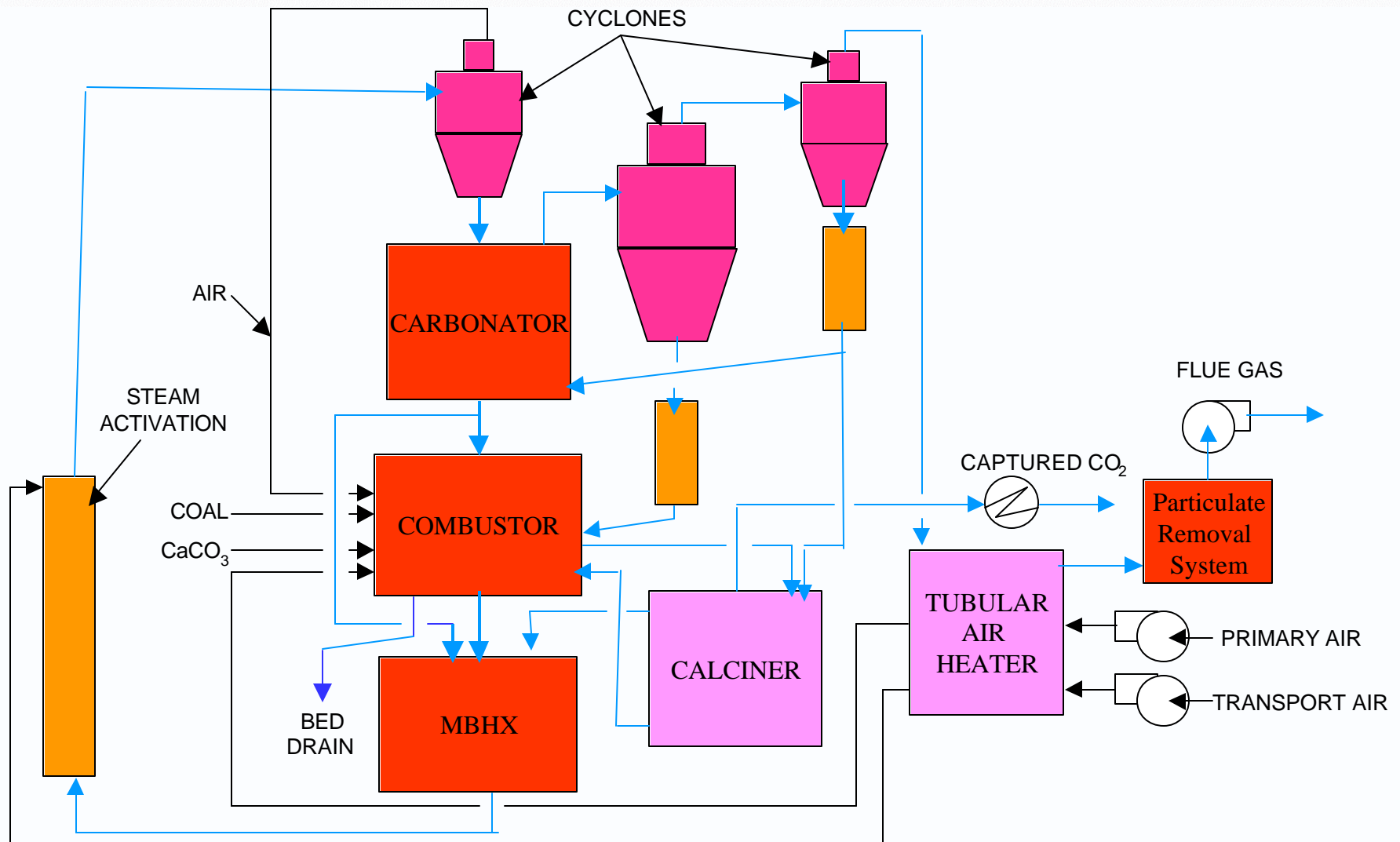


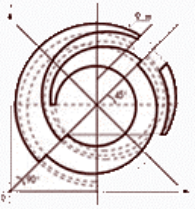
Potential combustion process with FBC's



High Temperature Carbonate Process for CO₂ Capture

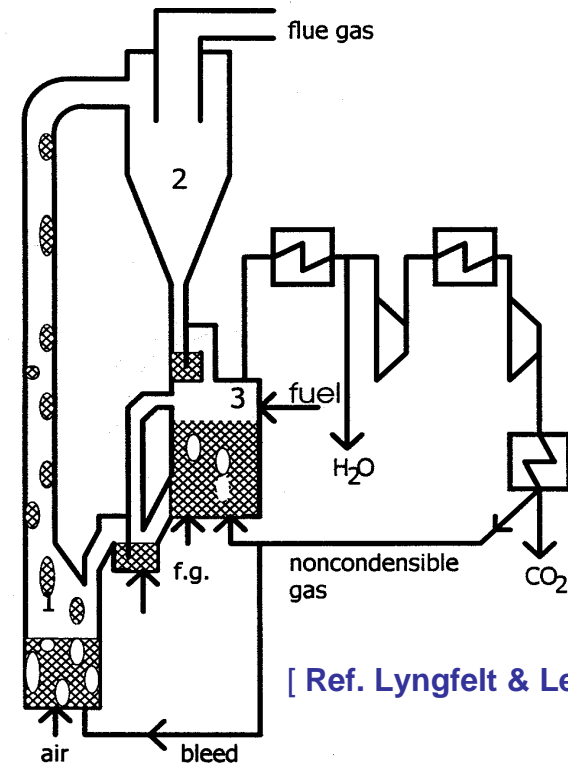
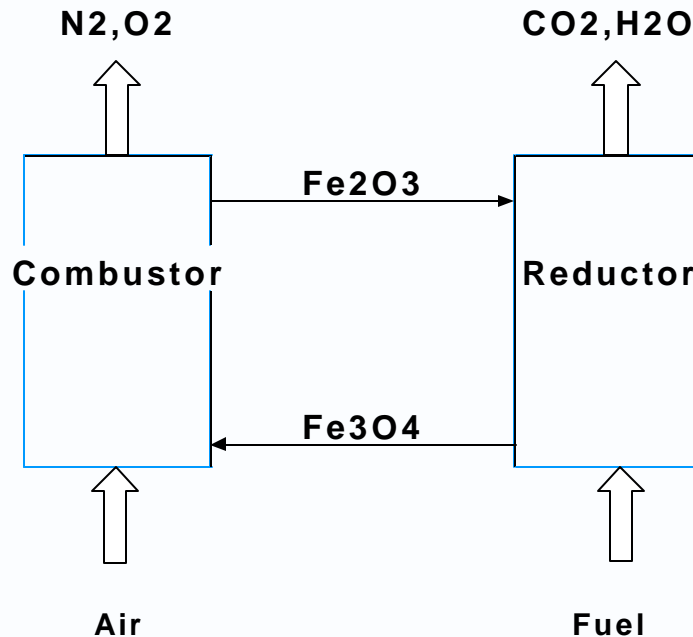
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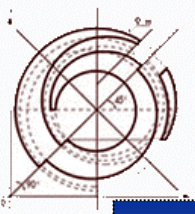
CO₂ Capture through Chemical Looping

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[Ref. Lyngfelt & Leckner]

- † Atmospheric Pressure
- † Oxygen carriers (Cu, Cd, Ni, Mn, Fe, Co)
- † Potential combustion process with interconnected FBC's



Environmental Controls

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Wet & Dry Flue Gas Desulphurisation



Mercury Control



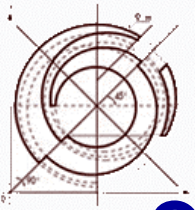
Wet and Dry Electrostatic Precipitator



De NOx



Technical Opportunity to Integrate with Combustion Process

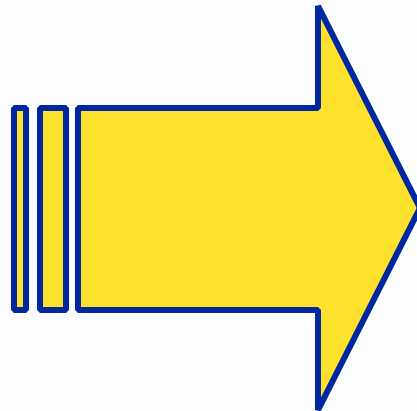


Roadmap for the Future

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CURC - Coal Utilization Research Council

An ad hoc group of coal suppliers, users, transportation, and equipment supplier organizations with the common interest to define and realize a vision for the future of coal power through industry/government collaboration



www.coal.org

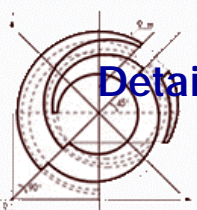


Advanced Combustion-based Steam Power Plant Roadmap

CURC December, 2001

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Attributes	Today	2006	2008	2010	2020
Capitall Cost(w/CO2 Removal)	1100(n/a)	1000(n/a)	900(<1400)	800(<1200)	800(<1000)
Efficiency(w/CO2 Removal)	40(n/a)	44(n/a)	45(>34)	46(>39)	50(>45)
Availability	95	95	95	95	95
SO2 Removal %	95+	98.5	98.5	99	99+
NOx (lbs/Mbtu)	0.1	0.1	0.05	0.05	0.01
Hg Removal %	30-90+	80-90+	90-95	90-95	95+
CO2 Removal %	n/a	n/a	n/a	90+	99
Waste Utilization	30	50	75	75	90+
Particulate Emis. (lb/Mbtu)	0.03	0.01	0.01	<.01	<.01
Steam Temperature	1100	1150	1200	1250	1400
Steam Pressure	3600	4000	4000	5000	5600
Development		Alloys for <1400; steam turbine; innov. Boiler & plant designs; APC integration (Sox/Hg/Part)	Valves for <1400; steam turbine; innov. Boiler & plant designs; APC integration (Sox/Hg/Part)	Valves for <1400; steam turbine; innov. Boiler & plant designs; APC integration (Sox/Hg/Part)	shift R&D to CO2 capture
Demonstration	1) 1100+ °F PC; 2) 300 MW CFB; 3) APC Int. CFB	1) 1150°F PC (700 MW); 2) Supercritical CFB	1) 1200°F PC (700 MW); 2) Adv. CFB (50 MW)	1) 1250°F PC (700 MW); 2) 600 MW CFB; 3) Adv. CFB (250 MW)	1) 1400°F PC (700 MW)
R&D cost	0	\$83	\$50	\$42	\$10
Demonstration Cost	0	\$445	\$270	\$580	\$220
Subtotal Cost	\$0	\$528	\$320	\$622	\$230
Total Cost					\$1,700



Details of Advanced Combustion-based Steam Power Plant Research and Development

CURC December, 2001



DEVELOPMENT

2006	Cost ⁽¹⁾	2008	Cost ⁽¹⁾	2010	Cost ⁽¹⁾	2020	Cost ⁽¹⁾	Totals ⁽¹⁾
Development and testing of alloys up to 1400 F	\$35	development and testing of valves for up to 1400	\$2	Development and testing of valves for up to 1401	\$2			\$39
Design studies of innovative plant designs	\$3	Design studies of innovative plant designs	\$3					\$6
Steam Turbine development	\$5	Steam Turbine development	\$5	Steam Turbine development	\$5			\$15
CFB cost reduction development	\$10	CFB cost reduction development	\$10					\$20
Advanced combustion systems development to enable high temp. cycles and future CO2 capture	\$20	Advanced combustion systems development to enable high temp. cycles and future CO2 capture	\$20	Advanced combustion system development to enable high temp. cycles and future CO2 capture	\$25			\$65
Integrated APC in CFB development	\$10	Integrated APC in CFB development	\$10	Integrated APC in CFB development	\$10	Integrated APC in CFB development	\$10	\$40
CO2 capture for combustion systems included in Carbon management roadmap ⁽²⁾	\$50	CO2 capture for combustion systems included in Carbon management roadmap ⁽²⁾	\$50	CO2 capture for combustion systems included in Carbon management roadmap ⁽²⁾	\$200	CO2 capture for combustion systems included in Carbon management roadmap ⁽²⁾	\$50	\$350
Subtotal Development	\$83		\$50		\$42		\$10	\$185

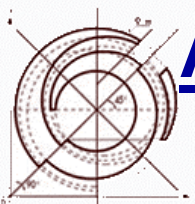
DEMONSTRATION

1150 F PC plant demo. (700 MW)	\$215	1200 F PC plant demo. (700 MW)	\$220	1250 F PC plant demo. (700 MW)	\$220	1400 F PC plant demo. (700 MW)	\$220	\$875
Supercritical CFB demonstration	\$200			600 MW CFB	\$180			\$380
Integrated SO2/Hg/Part. APC in CFB	\$30	Small demo. (50 MW) "adv. CFB repowering demo.	\$50	Large Demo. (250 MW) "adv. CFB demo.	\$180			\$260
		CO2 capture for combustion systems included in Carbon Management Roadmap ⁽²⁾	\$200	CO2 capture for combustion systems included in Carbon Management Roadmap ⁽²⁾	\$200	CO2 capture for combustion systems included in Carbon Management Roadmap ⁽²⁾	\$100	\$500
Subtotal Demonstration	\$445		\$270		\$580		\$220	\$1,515

Grand Total	\$528		\$320		\$622		\$230	\$1,700
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⁽¹⁾ Cost in millions U.S. Dollars

⁽²⁾ Costs included in Carbon Management Roadmap



Advanced Combustion Research Needs

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Flow

- ? bed fluid dynamics
 - ? clusters/solids distribution
 - ? attrition (coal/lime/ahs)
 - depreciation
 - fragmentation
 - ? fluidizing nozzles
 - ? 2 fluid modeling
 - dense phase
 - sub-routines/sub models
 - ? cyclone technology
 - separation technology
 - ? non-cyclone approaches
 - separation technology
 - ? input on size fuel/lime on combustion performance sulfur capture
 - ? flow measurement/control
 - neural network/fuzzy logic
 - ? agglomeration
 - ? flow sensors
 - density meters
 - spacial and temporal distributions
 - ? erosion/corrosion
 - modeling
 - refractory
 - ? bed mixing
 - ? scale-up issues
 - mixing
 - flow
 - pilot to utility scale
- erosion/co.
- ? $\frac{dp}{dt}$ ~ agglomerat ion meter

Materials

- ? coatings
- ? refractory
- ? materials

Heat Transfer

heat transfer as a function of (geometry, surface parameters)

solid to solid heat transfer
wall heat transfer
extended surface

moving bed heat transfer
hybrid beds
FBHE –fluid bed heat exchangers (external on recycle loop)

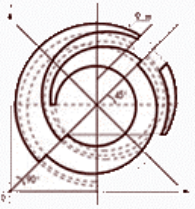
Cycles

- ? increase steam T&P
- ? combined cycles



Chemistry

- ? N₂O emissions
 - ? NO_x – staged combustion
 - ? post sulfur capture
 - ? advanced sorbents
 - ? Hg/air toxics/Cl
 - ? low excess air firing
 - ? condensables
 - ? polishing systems – SO₂
 - ? integrated APC – multipollutant
 - ? improved SNCR – technology application
 - ? effect of Cl – Hg & SO₂
 - ? reaction rates – char, CaSO₄, etc.
 - ? CaSO₃ CaSO₄ reactions/limitations
- post sulfur capture sorbents



Conclusions

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- ✍ Major efforts need to continue on the next generation options of supercritical designs, CFBs, and “advanced CFBs”.
- ✍ Environmental control development needs to be ongoing for SO_x, Hg, NO_x, and byproduct use.
- ✍ Innovative technology options for CO₂ capture/sequestration from combustion systems is now emerging and should be pursued.
- ✍ Government, Industry, and University collaboration is advocated to develop and demonstrate new coal generation options

Coal combustion-based power is an important option for which innovations are possible and needed.



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